

Hydrogen production by aqueous-phase reforming of glycerol on supported metal catalysts

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Introduction

The full environmental benefit of power generation from hydrogen fuel cells is only achievable if hydrogen is produced from sustainable resources such as biomass. Glycerol is the main biomass-derived product formed during bio-diesel production. Nowadays the worldwide trend of increasing production of bio-fuels results in an overproduction of glycerol. The hydrogen production from glycerol by the aqueous-phase reforming process at low temperatures and high pressures on various supported catalysts including Pt/Al₂O₃, Pd/Al₂O₃, Ni/Al₂O₃, Ru/Al₂O₃ and Rh/Al₂O₃ was studied.

Materials and Methods

The catalysts Pd/Al₂O₃, Pt/Al₂O₃, Ru/Al₂O₃, Rh/Al₂O₃ and Ni/Al₂O₃ were prepared by incipient wetness impregnation. The activity and selectivity of the catalysts for the aqueous-phase reforming of glycerol were studied in a laboratory reactor at 498 K 26.5bar and 513 K and 34.5bar, the concentration of glycerol was 1 - 10%wt.

Results and Discussion

The selectivities to hydrogen and alkanes at 489 K and 26.5 bar are shown in the figure 1.

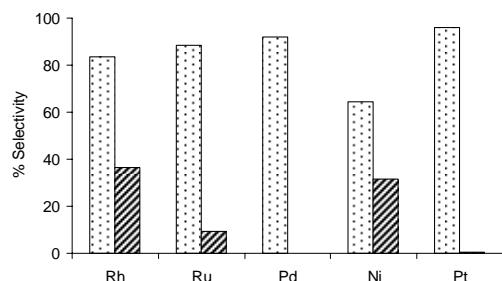


Figure 1. Hydrogen and alkane selectivity of the catalysts at 489 K and 26.5 bar. The hashed bar represents alkane selectivity and the white bars present hydrogen selectivity

The hydrogen selectivities of various metals supported on γ -Al₂O₃ were in the order Pt > Pd > Ru > Rh > Ni. The H₂ selectivities of Pt and Pd supported on γ -Al₂O₃ were above 90% with a

low alkane selectivity. The apparent activation energies of the metals supported on γ -alumina were in the order Pt < Pd < Ru < Ni < Rh.

The activity of the Pt/Al₂O₃ catalyst was studied for 2 weeks at 498 K and 29 bar, during this time the activity of the catalysts was almost constant as shown in Figure 2. The conversion of glycerol was close to 100% and less than 1000 ppm of CO were produced. Intermediate compounds such as methanol, ethanol, 1-propanol, propylene glycol, propanoic acid, acetol, acetic acid ethylene glycol, and small traces of untreated glycerol were present in the liquid phase.

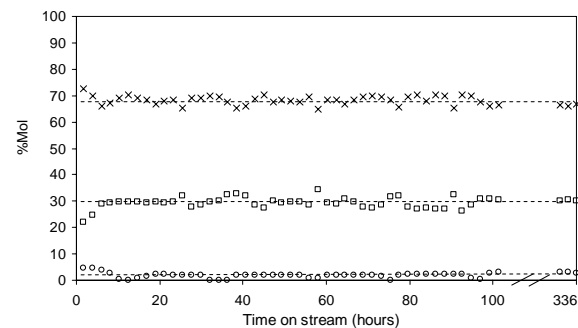


Figure 2. Concentration of gas products versus time H₂ (X); CO₂; (□); CH₄ (○)

Significance

The H₂ selectivity of Pt and Pd of more than 80% at 489 K and 513K together with the low alkane selectivity and the high long term stability indicates that Pt and Pd supported on gamma alumina could be a potential catalysts for the aqueous phase reforming of glycerol.

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